

| 1. PREAMBLE | | | |
|---------------------------|--------------------------|-------------------|--|
| Ship's name | GAS AEGEAN | | |
| Owners | CLARIN NAVIGATION | N CORP. | |
| | c/o: BENELUX OVER | SEAS Inc | |
| Flag – Registry | Liberia - Monrovia | | |
| Builder | STX Offshore & Shipb | uilding (S.Korea) | |
| Delivery | 28 JUNE 2012 | | |
| Class | KOREAN REGISTER | OF SHIPPING | |
| IMO No. | 9545209 | | |
| GT (International) | 9,134 | | |
| NT (International) | 2,745 | | |
| GRT (Suez) | 10,044.92 | | |
| NRT (Suez) | | 9,297.78 | |
| GRT (Panama) | | 7.712.00 | |
| LWT (MT) | | 4,934.60 | |
| Is vessel approved? | | | |
| USCG | | Yes | |
| IMO | | Yes | |

| 2. HULL | | | | |
|--------------------------|----------------|-------------|-------------------|--------------|
| | Ме | tres | Feet | |
| LOA | 12 | 0.4 | | 395.01 |
| LBP | 11 | 2.4 | 368.76 | |
| Breadth | 19 | 9.8 | 64.96 | |
| Depth | 1 | 1.2 | | 36.74 |
| Air draft (fm Summer LL) | 2 | 7.8 | | 91,18 |
| | Draft (m) | | Corresponding DWT | |
| Tropical | 9 | .00 | 10,821,50 | |
| Summer | 8 | .81 | 10,388,00 | |
| Winter | 8.63 | | • | 10,042.20 |
| TPC fully loaded (MT) | | 20.4 | | |
| Estimated Mean draft | with full bunk | ers and 98% | cargo & | full bunkers |
| Cargo | Mean draft (| m) DV | NT | displacement |
| Propane | 7.6 | 7,7 | 7 58 | 12,800 |
| Butane | 7.8 | 7,9 | 955 | 12,997 |
| Ammonia | 8.4 | 9,4 | 195 | 14,538 |
| VCM | 7.4 | 7,4 | 125 | 12,468 |
| Propylene Oxide | 7.4 | 7,4 | 178 | 12,520 |

| 3. COMMUNICATION EQUIPMENT | | |
|----------------------------|-------|--|
| International call sign | D5AO9 | |



| Radio station | 636015415 |
|---------------|----------------------------------|
| Inmarsat F77 | |
| - Telephone | 765101528 |
| - Telephone | 765101529 |
| - Telefax | 765101530 |
| - Telex | |
| Inmarsat C | 463712494 |
| MMSI | 636015415 |
| Cell phone | - |
| E-Mail | master.gasaegean@amosconnect.com |

| 4. MACHINERY | | | | |
|--|---|-------------------|------------|--|
| | Main E | ingine | | |
| Maker/model | STX/MAN-B&W (7S3 | B5MC-C Mk7) | | |
| MCR | 5,180KW / 173 RPM | | | |
| Grade fuel used | I.F.O 180/280/380. & | M.D.O 30/60/70. | | |
| | Auxiliaries | | | |
| Type/Model | Four stroke diesel e | ngine - MAN 6L21/ | 31 | |
| Maker | STX Engine Ltd (S.F | | | |
| Output(KW/RPM) | 3 x 1,176KW @ 90 | | | |
| Generator | 3 x 1,100 KW /450V | | | |
| Grade fuel used | I.F.O 180/280/380 8 | M.D.O 30/60/70. | | |
| | Spe | ed | | |
| Guarantee average | loaded/ ballast spe | ed (kt) | 15,2 | |
| Draft at Guarantee | Draft at Guarantee average loaded/ ballast speed (m) 7,65 | | | |
| | Consun | nption | | |
| Consumption Consumption | | | | |
| | at sea at port | | | |
| | jine (IFO) | 17.8 MT/day | - | |
| | ines (IFO) | 2.4 MT/day | 2.6 MT/day | |
| Number of A/E in use | | One(1) | Two(2) | |
| MDO Consumption alongside in port 2.4 MT/Day | | | 2.4 MT/Day | |
| Inert Gas plant whe | <u> </u> | - | - | |
| Boiler consumption (MT/day) 1.5 | | | | |
| Permanent bunkers capacity (Excl. daily service tanks) @ 98% | | | | |
| HFO (MT) | 937 | | | |
| MDO (MT) | 127 | | | |

| 5. CARGO INSTALLATION | |
|----------------------------|------------------|
| Re-liquefaction plant Type | Compression type |

GAS FORM- C



Minimum temperature can maintain

-48.4° C (propylene)

| Tank No. | Сара | cities | n-C4 0.605 @ - | C3 0.582 @ -41.5° C | NH3 0.682 @ -33.4° C | Butadien e 0.653 @ |
|-------------|---------------------|--------------------|-------------------|------------------------|-------------------------|-----------------------|
| | 100% M ³ | 98% M ³ | 5° C | | | -5 °C |
| 1 | 4,551.05 | 4,460.03 | 2,698.30 | 2,595.70 | 3,041.70 | 2,912.40 |
| 2 | 4,550.99 | 4,459.97 | 2,698.30 | 2,595.70 | 3,041.70 | 2,912.40 |
| Total | 9,102.02 | 8,920.00 | 5,396.60 | 5,191.40 | 6,083.40 | 5,824.80 |

Carried Products

Propene (Propylene), commercial Propane*, Propane/Butane mixtures, Anhydrous Ammonia, Vinyl Chloride Monomer, i-Butane, Butene (Butylene), Butadiene, Acetaldehyde, Dimethylamine, Ethyl Chloride, Diethyl Ether**, Ethene Oxide/Propene Oxide(max. 30%W-%E.O)**, isoprene(monomer), isopropylamine**, Monoethylamine**, Propene Oxide, Vinyl Ethyl Ether**

Notes:

(*) Propane/Ethane mixtures:

Maximum ethane percentage for commercial Propane in liquid phase at saturated temperature is 2.5 mol-% Ethane at 1.013bar-abs

(**) Maximum allowable quantity of cargo per tank should not exceed 3,000 m³ in any one tank according to IGC Ch.17 §11

Cooling before loading

(for fully-refrigerated vessels what quantity of cargo is needed and which is the corresponding time to pre-cool the tanks and have them ready to load?)

| | MT | Hrs |
|-----------|----|-----|
| BUTANE | 37 | 35 |
| PROPANE | 41 | 65 |
| BUTADIENE | 35 | 35 |
| AMMONIA | 25 | 45 |
| VCM | 42 | 30 |

| 6. CARGO TANKS | | | |
|---|--------------------|-----------------------------|--|
| Туре | Independent Cylind | rical type-C with hemi-ends | |
| Material | | 13MnNi63 | |
| MARVS | | IMO 5.8 bar-g | |
| WARVS | | USCG 3.55 bar-g | |
| Maximum Vacuum | | about - 0.25 bar | |
| Minimum pressure | | about 0.75 bar | |
| Minimum temperature acceptable in tanks | | -48° C | |
| Maximum Specific Gravity | | 972 kg/m ³ | |
| Maximum Loading | g rate – m³/hour | 900 | |
| Number of deck tanks | | N/A | |

7. CARGO PUMPS



| Number/Type | 2 v F | lectric driven v | ertical Deen-well | numns | |
|---|---|------------------|---|---------------------------|--|
| | 2 x Electric driven vertical Deep-well pumps (450 m ³ /h @ 120m mlc) | | | | |
| Maker | | (| <u> </u> | y-Svanehoj | |
| Location | | | | k's dome | |
| Max permissible | specific gravi | tv | | kg/m³ | |
| Cargo remaining | | | | | |
| after total comp | | _ | 0,075m³/per | Tank in sump | |
| Cargo remaining | | | Liquid | 6 m³ | |
| (heel) after com | pletion pumpii | ng | Vapour | Subject to tank condition | |
| Total head wher booster pump | n working in se | ries with | 240 | mlc | |
| | | | riven horizontal centrifugal pumps | | |
| (number/type) (2 | | | 225 m ³ /h @ 120m mlc | | |
| Maker | | | Hamworthy-Svanehoj | | |
| Stripping | | | | | |
| Stripping system | | | Pressurizing | | |
| Time required for all traces of liquid cargo | | | , | ank condition | |
| | Loading Rates | | | | |
| Loading rate (stopressure + vapor | | | 545 MT /h | | |
| Loading rate (storage tank at atmospheric pressure) – PROPANE* | | | 525 MT/h | | |
| Loading rate (storage tank at atmospheric pressure) – AMMONIA * | | | 615 MT/h | | |
| Loading rate (storage tank at atmospheric pressure) – BUTADIENE* | | | 580 MT /h | | |
| Loading rate (provapour return line | essurized storaç | ge tank with | Subject to cargo temperature and ambient conditions | | |
| Loading rate (pressurized storage tank with vapour return line) – AMMONIA | | | Subject to cargo temperature and ambient conditions | | |

(*)Note: for pressure or semi-refrigerated vessels using the cargo heater with sea temperature +15° C

| Time for discharging full cargo using all pumps against no backpressure | | | |
|---|--------------------|---------------------|--|
| | With vapour return | Without vapour | |
| | line (hours) | return line (hours) | |
| Discharging rate (atm) | 10 | 10 | |
| Discharging rate (1 bar) | 12 | 12 | |
| Discharging rate (5 bars) | - | 12 | |
| Discharging rate (10 bars) | - | 20 | |

| 8. CARGO COMPRESSORS | |
|----------------------|--------------------------------------|
| Number/Type | 2 x (two stage piston type-Oil free) |



| Maker/Model | | Sulzer Burckhardt 2K-160-2H | |
|------------------------|-----------|-----------------------------|---------------------|
| Total Swept volume | | 1200 m ³ / hr | |
| Can re-liquefy VCM | | YES | |
| | | Propane Ammonia | |
| | Prop | oane | Ammonia |
| Refrigeration Capacity | Abt 910kW | oane | Ammonia Abt 1269 kW |

| 9. INERT GAS SYSTEM | | | |
|--|----------------------------|--|--|
| Does the vessel use inert gas? | YES | | |
| Method | PSA System/ pressure swing | | |
| | adsorption | | |
| Maker | CARBONTECH Gmbh | | |
| Fuel used | N/A | | |
| Does the vessel produce inert gas? | YES | | |
| Туре | Nitrogen | | |
| Daily production | 750 m³/hr @ 99.5 % vol | | |
| Composition | n of inert gas | | |
| Garbon dioxide | N/A | | |
| Oxygen max. | Max. 2% - Min. <0,1% | | |
| Garbon monoxide max. | N/A | | |
| Hydrogen max. | N/A | | |
| Nitrogen | 98% to 99,9% | | |
| Soot | N/A | | |
| Suphur oxides max. | N/A | | |
| Dewpoint -50° C | | | |
| State if any shore supply of liquid nitrogen may be required | | | |
| May be required for pumping tanks prior to loading butadiene and ammonia | | | |
| What quantity? N/A | | | |

| 10. GAS FREEING | | | | |
|--|-------------------------------|---------|------------------------------|--|
| Can this operation be carried out at sea? YES | | | YES | |
| | State method incl. | all det | ails | |
| For LPG | Nitrogen by vessel's own plan | t, aera | tion by air compressor | |
| For NH ₃ | Nitrogen by vessel's own pl | ant, ve | entilation by air compressor | |
| Advi | se time required and consun | nption | of inert gas if any | |
| From LPG abo | From LPG about Apx 24 hr | | | |
| From NH ₃ Apx. 24 hr | | | Apx. 24 hr | |
| Is the vessel equipped with inert gas blower? N/A | | | N/A | |
| Capacity N/A | | | N/A | |
| Ventilation fan N/A | | | N/A | |
| 11. CHANGING GRADE | | | | |
| Can this opera | ation be carried out at sea? | | YES | |



State method used and time required for charging from NH₃ to LPG and vice versa, to reach 50 ppm to previous cargo in tanks atmosphere, the tanks being dry and free of moisture (dewpoint plus 10° C)

| tanks being dry and free or moisture (dewpoint plus 10°C) | | | |
|---|--------------------------------|--|--|
| From NH ₃ to LPG | Nitrogen production PSA System | | |
| Time required | Abt. 48h | | |
| From NH ₃ to LPG | Nitrogen production PSA System | | |
| Time required | Abt. 48h | | |
| Can vessel reduce in tank atmosphere | | | |
| and gas installation concentration of | YES | | |
| previous cargo below 50 ppm? | | | |
| Method used, time required and extra | Nitrogen Production, time | | |
| shore supply if any | depending on cargo conditions, | | |
| | shore supply possible | | |
| How can it be checked that no liquid gas | Check level indicators, open | | |
| remain onboard | drains at low points | | |

| 12. CARGO HEATER | | | |
|---|-----------------------------|-----------|--|
| Cargo Heater | YES | | |
| Maker | TGE Marine Engineering Gmbh | | |
| Туре | Shell/tube | | |
| Discharging rate for C3 & NH3 to be brought | 230 MT/hr | | |
| fm atmospheric pressure to -5° C @ S.W 15° C | AMMONIA | 150 MT/hr | |
| State discharging rate for propane with 2.5 m brought from -44oC to -5oC at sea temperatu | 350 MT/hr | | |

| 13. CARGO VAPORIZER | |
|--|------------------|
| In case of need of vapor gas during discharge, can | Yes by cargo |
| vessel produce its own if no shore gas available? | heater/vaporizer |

| 14. REFRIGERATING APPARATUS | | |
|-----------------------------|--------------------------------------|--|
| It is independent of cargo? | YES | |
| | Two(2) grade re-liquefaction systems | |

| 15. MEASURING APPARATUS | | | |
|-----------------------------------|--------------------------------------|--|--|
| What gauges onboard | Level/pressure/temperature | | |
| Location and type | Float type level gauges/P& T sensors | | |
| Number of temperature | 10 pec | | |
| sensors/gauges per tank | | | |
| Number of pressure sensors/gauges | ges 3 pcs | | |
| on tank | | | |
| 16. SAMPLES | | | |
| Where samples can be taken? | Five(5) vapours samples inside | | |



| | tank, one closed sampling liquid sample by circulation |
|---------------------------------------|--|
| Are sample bottles available onboard? | YES |

| 17. CARGO LINES | |
|---|----------------------|
| Is vessel fitted with midship manifolds | YES |
| Number of lines on each side | 2 x Liquid (6" & 8") |
| | 300A |
| | 2 x Vapour (4" & 6") |
| | 300A |
| Lines Configuration | L-V-V-L |
| Distance from cargo manifold to bow | 56,700mm |
| Distance from manifold to stern | 63,600 mm |
| Height upper cargo manifold above main deck | 3,000 mm |
| Height above Summer Draft mark | 5,400 mm |
| Height upper cargo manifold waterline when LWT | 10,720 mm |
| Height upper cargo manifold above waterline when in ballast | 9,130 mm |
| Distance manifold from ship's rail | 2,100 mm |
| Distance between liquid lines | 4,200 mm |
| Distance between vapour lines | 1,400 mm |
| Distance between loading and vapour return connections | 1,400 mm |
| Is vessel fitted with stern discharge | N/A |
| Is vessel fitted with fore discharge | N/A |

Note: Above distances from center line of liquid and vapour crossovers

| Dimension of lines | | | | |
|--------------------|-----------|--------------|-----------------|--|
| | Dia | meter | Flange size | |
| Liquid (P/S) | 6' | ', 8'' | ANSI #300 | |
| Vapour | 4' | ', 6'' | ANSI #300 | |
| Booster | 1 | N/A | N/A | |
| | What redu | cers onboard | | |
| Number | Diameter | Length | Pressure rating | |
| 1 | 8" x 8" | 500mm | (300# x 300#) | |
| 2 | 6" x 8" | 500mm | (300# x 300#) | |
| 3 | 6" x 6" | 500mm | (300# x 300#) | |
| 4 | 4" x 6" | 500mm | (300# x 300#) | |
| 5 | 8" x 10 | 500mm | (300# x 300#) | |
| 6 | 8" x 6" | 500mm | (300# x 300#) | |
| 7 | 6" x 6" | 500mm | (300# x 300#) | |
| 8 | 6" x 8" | 500mm | (300# x 300#) | |
| 9 | 6" x 4" | 500mm | (300# x 300#) | |



| 10 | 6" x 3" | 500mm | (300# x 300#) |
|----|----------|-------|---------------|
| 11 | 4" x 4" | 500mm | (300# x 300#) |
| 12 | 4" x 3" | 500mm | (300# x 300#) |
| 13 | 8" x 10 | 500mm | (300# x 150#) |
| 14 | 8" x 8" | 500mm | (300# x 150#) |
| 15 | 8" x 6" | 500mm | (300# x 150#) |
| 16 | 6" x 8" | 500mm | (300# x 150#) |
| 17 | 6" x 6" | 500mm | (300# x 150#) |
| 18 | 6" x 4" | 500mm | (300# x 150#) |
| 19 | 6" x 3" | 500mm | (300# x 150#) |
| 20 | 4" x 6" | 500mm | (300# x 150#) |
| 21 | 4" x 4" | 500mm | (300# x 150#) |
| 22 | 4" x 3" | 500mm | (300# x 150#) |
| 23 | 6" x 12" | 500mm | (300# x 300#) |

| 18. LIFTING APPLIANCES | | | | |
|--|--|---------------------------------|--|--|
| Where situated | Aft | Amidship | | |
| Number and lifting capacity | Provision and engine part handling crane(1.5t SWL) | hose handling crane (4t SWL) | | |
| Max. distance from ship's side of lifting hook | max 6,000mm | max 15,000mm | | |

| 19. HOSES | | | | | |
|--------------------------------------|---------|----------|----------|-----------|--|
| For what products are hoses suitable | | | | | |
| Number | Length | Diameter | Working | Flange | |
| | | | pressure | | |
| Purging hose | 6,000mm | 4" | 12 | ANSI #150 | |
| Drain hose | 6,000mm | 1" | 35 | ANSI #300 | |

| 20. SPECIAL FACILITIES | | |
|---------------------------------------|-------------------------------|--|
| How many grades can vessel segregate? | | |
| Indicate systems | Two(2) grades - if compatible | |
| Is vessel able to load/discharge two | YES | |
| or more grades simultaneously? | | |
| Can vessel sail with slack tanks? | YES | |
| Is vessel fitted with purge tank? | NO | |